# Basics of Creating Latex Particles with Controlled Size and Chemistry

## Session 1

- Course introduction and overview
- Course objectives and expectations of participants
- Basic chemical mechanisms and modes of reaction for emulsion polymers
  - 1. Free radical polymerization reactions
  - 2. Polymer chain characteristics, radius of gyration, entanglements
  - 3. Chain structure linear, branched, grafted, crosslinked
  - 4. Reaction rates in free radical polymerization
    - Homopolymerization free radical and monomer concentrations, influence of temperature and viscosity
    - Copolymerization reactivity ratios, cross-termination, copolymer composition control, chain transfer to polymer reactions
  - 5. Molecular weight control
    - Chain growth and stopping events, number average chain length
    - Molecular weight distributions, most probable distribution, dependence on monomer and radical concentrations, chain transfer agent
  - 6. Modes of reaction
    - Batch reactions time dependencies, reaction rates
    - Semi-batch reactions monomer feeding profiles, control of monomer concentrations, copolymer composition control, temperature variations, residual monomers

# Session 2

- Creating polymer particles in emulsion polymerization
  - 1. Chemical and physical mechanisms involved in batch reactions
  - 2. Physical chemistry of surfactant micelles
  - 3. Initiation of radicals in water phase, z-
  - mer concept, radical entry
  - 4. 3-time intervals of reaction, distinctive boundaries between intervals
  - 5. Homogeneous nucleation of particles
  - (without micelles)
  - 6. Particle size control
    - Ab initio
    - Growth from seed
    - Control of particle size
  - distribution Details for rates of reaction during emulsion

## polymerization

- 1. Smith-Ewart approach quantitative difference equations
  - Cases for nbar = 1/2 --instantaneous termination in latex particles
  - $\circ$  Cases for nbar < 1/2 --- radical exit
  - Cases for nbar > 1/2 --- diffusion controlled termination, pseudo bulk
- 2. Batch reaction rates vs. time of reaction (conversion), Intervals I, II and III
- 3. Semi-batch processing alternatives
  - Why use semi-batch?
  - Effect on [M] and on polymer viscosity in particles
    - a) How far can radicals penetrate into particles?
    - b) How do polymer particles grow? Accretion? Monomer swelling?
    - c) Effect of polymer T<sub>g</sub> and [M] on reaction rates; diffusion controlled termination, chain transfer to polymer in acrylates
    - d) Residual monomer

- 4. Initiator systems
  - Thermal dissociation
    - a) Water phase initiation, oil phase initiation
    - b) Initiator end groups, especially for water phase initiation
    - c) Dead end polymerization, feeding initiator during process
  - Redox systems
    - a) Commonly used oxidant/reductant pairs
    - b) Reactivity of oxygen vs. carbon centered radicals
    - c) Initiator efficiencies (oil phase, water phase)
  - Methods of addition distinguish between addition during polymerization process and during the finishing operation (to remove residual monomer)

## Session 3

#### • Details for latex particle size control

- 1. Ab initio processes in batch process
  - Micellar mechanism
  - CMC values; temperature and ionic strength effects
  - Interval I in Harkins mechanism of particle formation
    - a) Time and conversion duration of this interval
    - b) Possible size difference between youngest and oldest particles
  - Intervals II and III in Harkins mechanism
    - a) Particle growth during interval II; monomer concentration in particles
    - b) Interval III (no growth); finishing the polymerization
  - Colloidal stability during Intervals I and II
    - a) Controlling surfactant coverage
    - b) Consequences of too much surfactant (secondary nucleation)

- c) Consequences of too little surfactant during growth interval – coagulation
- 2. *Seeded* latex particle growth
  - Size of seed vs. final, desired size, stage ratio
  - Residual surfactant and initiator in seed latex possible need for extra
  - o Monomer feed alternatives
    - a) Batch process; [M] in particles at start of seeded reaction
    - b) Semi-batch; *starved* and flooded conditions
    - c) Power feeds for some copolymer systems
    - d) Reaction rates during semibatch operations

#### • Details for molecular weight control

1. Kinetic chain length, *<*X<sub>N</sub>*>*; special considerations for emulsion polymerization

- Radical entry rate
- Chain termination in particles; long-short termination
- Chain transfer to monomer effects (only in batch reactions)
- Chain transfer to external agents
  - a) Solubility in water issues
  - b) Transport to latex particles
  - c) Chain transfer constants

#### Session 4

# • Details for molecular weight control, continued

- 2. Molecular weight distributions (MWD)
  - Linear chains; changing conditions of [M] and radical entry rates
  - Branching reactions; chain transfer to polymer, addition of divinyl monomers
  - Crosslinking reactions; natural/inherent as in acrylates and dienes; with added divinyl monomers
- Details for copolymer composition control
- 1. Batch reactions
- 2. Semi-batch reactions
- Introduction to colloidal stability

 Electrostatic stability mechanism; temperature and ionic strength issues
Steric stability; entropy considerations, non-ionic stabilizers

• Review of important lessons learned and conclusion of workshop